Cargèse Summer School 2018

Bioenergetics and Geomicrobiology

(Are microbes better at thermodynamics than geochemists?)

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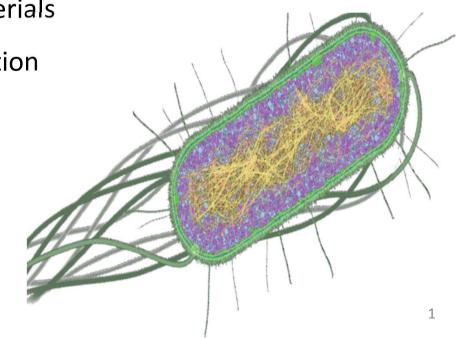


Geomicrobial Activity

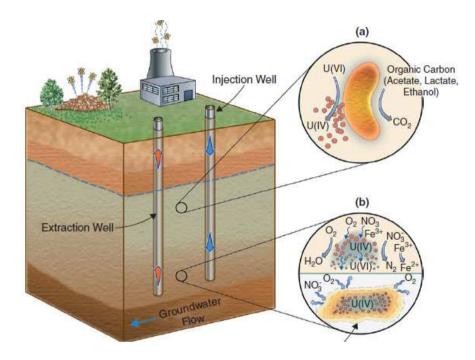
- Cycling of carbon and nutrients (N, S, P, K, Si, Ca, Fe, ...)
- Weathering, soil formation, soil fertility, water quality
- Organic matter decomposition, transformation and preservation
- Production greenhouse (CO₂, CH₄, N₂O) and other reactive gases
- Biomineralization, bio(nano)materials
- Natural attenuation, bioremediation
- Biotechnology

. .

• Green (bio)chemistry

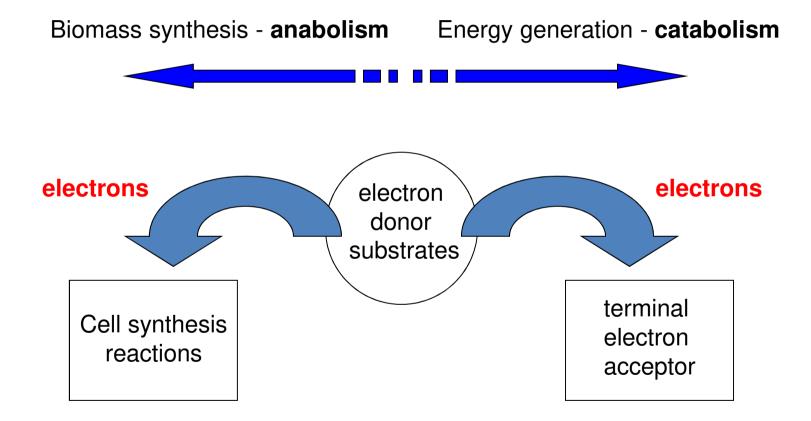


Geomicrobial Activity in the Subsurface



- Microbial ecosystems
- Ecological interactions
 - competition, syntrophy,
 - predation, energy flow
- Complex reaction networks
 - biotic-abiotic
- Energy-limited environments

Life = Redox Chemistry



Example

Aerobic cell growth on citric acid: macrochemical reaction:

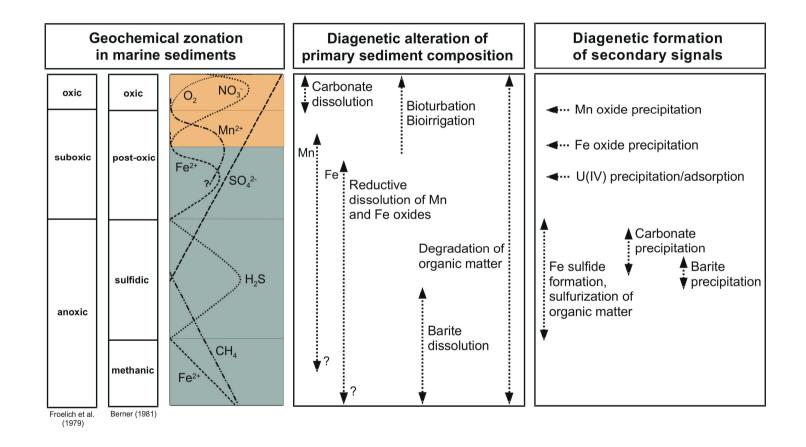
$${}^{+1}_{aC_{6}H_{8}O_{7}} + bO_{2} + cNH_{4}^{+} \longrightarrow dCH_{2}O_{0.6}N_{0.2} + eCO_{2} + fH^{+} + gH_{2}O$$

$${}^{-0.2}_{new biomass} + eCO_{2} + fH^{+} + gH_{2}O$$

Citric acid ($C_6H_8O_7$): both electron donor for energy production and for biomass synthesis.

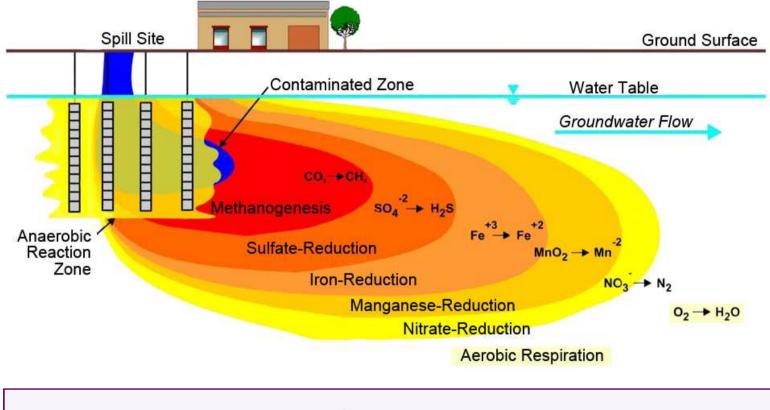
Growth yield: Here: $Y_G = d/6a$ (mol C/mol C)

Redox Zonation



http://www.awi.de/fileadmin/user_upload/Research/Research_Divisions/Geosciences/Marine_Geochemistry

Redox Zonation \rightarrow Thermodynamics



Redox zonation:

subsurface microbial communities optimize catabolic energy production

Microbial Kinetics

Microbial growth: *Monod kinetics*



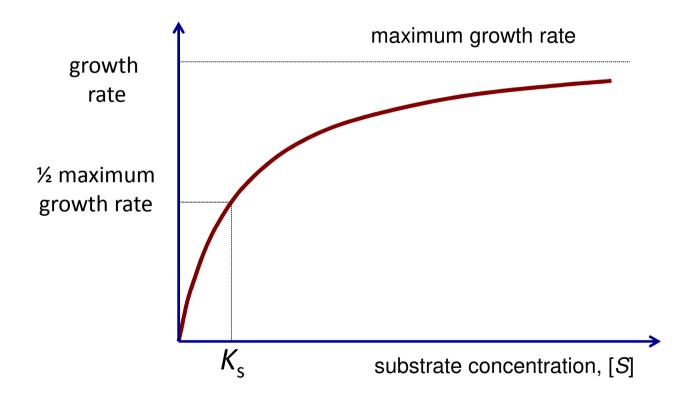


- X: biomass
- μ : specific growth rate

 μ_{\max} : maximum μ

- S: limiting (growth) limiting
- $K_{\rm s}$: half-saturation constant

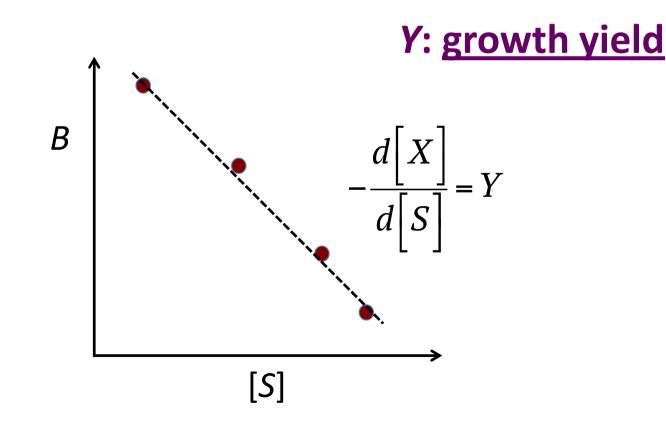
Saturation Kinetics



Growth Kinetics \rightarrow Geochemical Kinetics

Michaelis-Menten kinetics (substrate utilization):

$$-\frac{d[S]}{dt} = \frac{\mu_{\max}}{Y} \cdot X \cdot \frac{[S]}{K_s + [S]}$$



Example: Sulfate Reducers Growing on H₂

Electron donor:

$$\left[H_{2} \rightarrow 2H^{+} + 2e^{-} \right] \times 4$$

Electron acceptor:

$$\mathrm{SO}_4^{2-} + 8e^- + 10\mathrm{H}^+ \rightarrow \mathrm{H}_2\mathrm{S} + 4\mathrm{H}_2\mathrm{O}$$

Catabolic reaction:

$$SO_4^{2-} + 4H_2 + 2H^+ \rightarrow H_2S + 4H_2O$$

Catabolic Reactions & Thermodynamics

$$SO_4^{2-} + 4H_2 + 2H^+ \rightarrow H_2S + 4H_2O$$

 $\Delta G < 0:$ energy yielding reaction
 $\Delta G \ge 0:$ energy demanding reaction

Catabolic reaction: $\Delta G < 0$

$$\Delta G = \Delta G^0 + RT \ln Q$$

Gibbs Energy of Reaction

$$\Delta G = \Delta G^0 + RT \ln Q$$

$$\Delta G^{0}$$
: standard state Gibbs energy ($a_{i} = 1$)
 $\Delta G^{0} = f(P,T)$
 $\Delta G^{0} = -RT \ln K_{eq}$

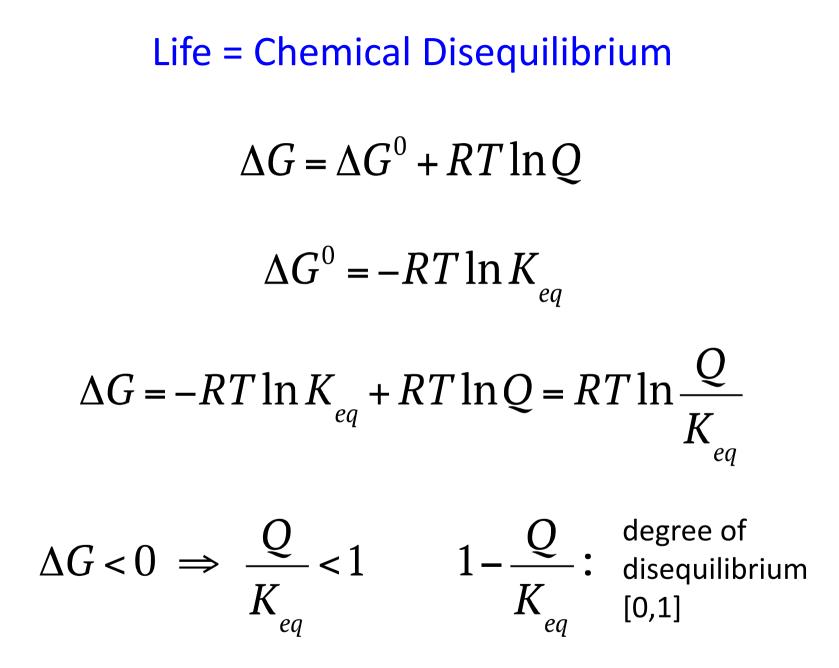
Q: reaction quotient

$$Q = \frac{\Pi a_{\text{product } i}^{v_i}}{\Pi a_{\text{reactant } j}^{v_j}}$$

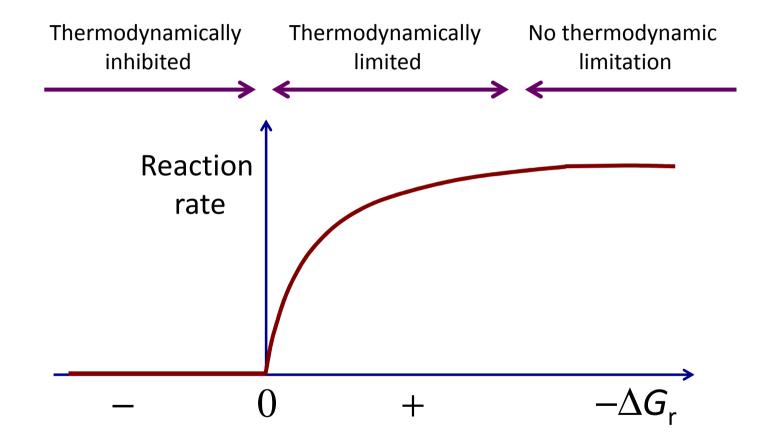
a: activity *v*: stoichiometric coefficient Example: Sulfate Reducers Growing on H₂

$$SO_{4}^{2-} + 4H_{2} + 2H^{+} \rightarrow H_{2}S + 4H_{2}O$$
Aqueous solute: $a_{SO_{4}^{2-}} \approx [SO_{4}^{2-}]; a_{H_{2}S} \approx [H_{2}S]$
Hydrogen ion: $a_{H^{+}} = 10^{-pH}$
Volatile species: $a_{H_{2}} \approx P_{H_{2}}$
Pure solid: $a_{solid} = 1$ solvent: $a_{H_{2}O} \approx 1$

$$Q = \frac{[H_{2}S]}{[SO_{4}^{2-}]P_{H_{2}}^{4}(10^{-pH})^{2}}$$



Kinetics and Thermodynamics



Thermodynamic Limitation

Example: Sulfate reducing bacteria growing on H₂

Classical "Monod" kinetics:

$$-\frac{d\left[SO_{4}^{2^{-}}\right]}{dt} = \frac{\mu_{\max} \cdot X}{Y} \cdot \left\{\frac{\left[H_{2}\right]}{K_{H_{2}} + \left[H_{2}\right]} \cdot \frac{\left[SO_{4}^{2^{-}}\right]}{K_{SO_{4}} + \left[SO_{4}^{2^{-}}\right]}\right\}$$

With thermodynamic limitation:

$$-\frac{d\left[SO_{4}^{2^{-}}\right]}{dt} = \frac{\mu_{\max} \cdot X}{Y} \cdot \left\{\frac{\left[H_{2}\right]}{K_{H_{2}} + \left[H_{2}\right]} \cdot \frac{\left[SO_{4}^{2^{-}}\right]}{K_{SO_{4}} + \left[SO_{4}^{2^{-}}\right]}\right\} \cdot F_{T}$$

Thermodynamic Driving Force, F_{T}

$$\Delta G_{cat}^* > 0: \quad F_T = 0$$

$$\Delta G_{cat}^* < 0: \quad F_T \text{ between 0 and 1}$$

$$\Delta G_{cat}^* << 0: \quad F_T \to 1$$

$$\Delta G_{\text{cat}}^* = \Delta G_{\text{cat}} + \Delta G_{\min} \text{ where } \Delta G_{\min} > 0$$

Model 1*: $\Delta G_{\min} = m \cdot \Delta G_{\text{ATP}}$
Model 2#: $\Delta G_{\min} = F \cdot \Delta \Psi$

*Jin Q. and Bethke C.M. (2003) *Appl. Environ. Microbiol.* **69**, 2340-2348 #LaRowe D.E. et al. (2012) *Geochim. Cosmochim. Acta* **90**, 96-109

Thermodynamic Driving Force, F_T

Model 1: Transition State Theory

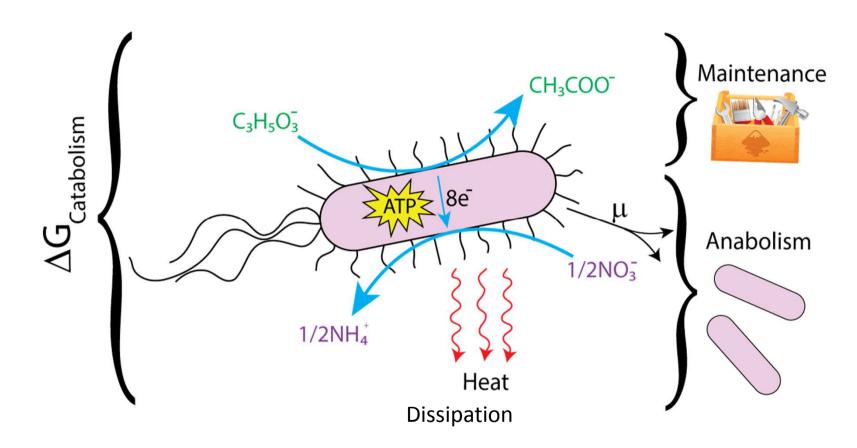
$$\begin{split} \Delta G_{\text{cat}} + m \Delta G_{\text{ATP}} < 0: \quad F_{T} = 1 - \exp\left(\frac{\Delta G_{\text{cat}} + m \Delta G_{\text{ATP}}}{\chi R T}\right) \\ \Delta G_{\text{cat}} + m \Delta G_{\text{ATP}} \ge 0: \quad F_{T} = 0 \end{split}$$

Model 2: Fermi-Dirac Statistics

$$F_T = \frac{1}{e^{\frac{E}{RT}} + 1}$$
 where $E = \Delta G_{cat} + F \Delta \Psi$

Active bacteria: $\Delta \Psi \ge 100 \text{ mV}$

Cellular Energy Balance



Catabolic energy production = growth + dissipation + maintenance

Anabolic Energy Demand

Anabolism (ANA):

Catabolism (CAT):

carbon source + nutrients (N, P, ...) + energy \rightarrow 1 C-mol biomass

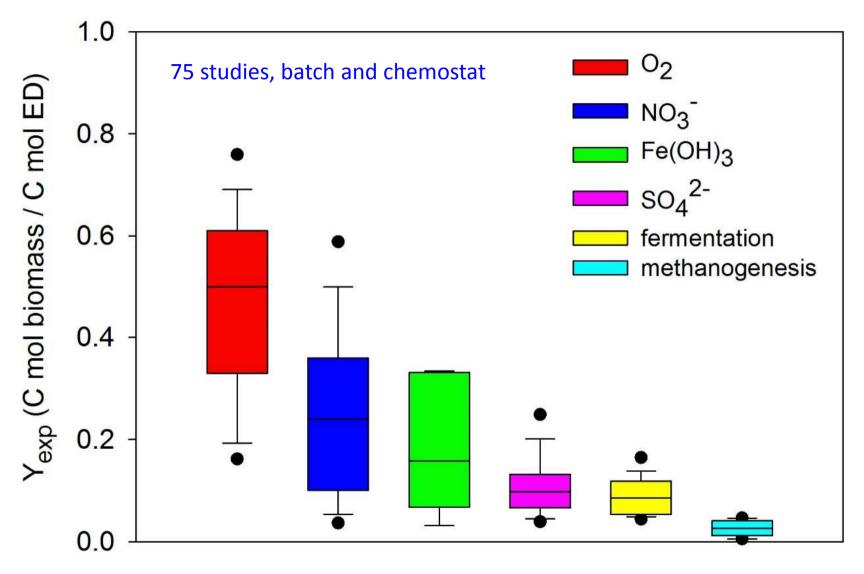
electron donor + electron acceptor \rightarrow products + energy

Metabolic reaction (MET): MET = ANA + $\lambda_{cat} \bullet CAT$

 λ_{cat} : number of times the catabolic reaction must proceed in order to build 1 C-mol biomass

λ_{cat} is directly related to the growth yield!

Thermodynamics \rightarrow Growth Yields



Smeaton C. and Van Cappellen P. (2018) GCA – under review.

Example: Iron Reducers Growing on Acetate

Anabolic reaction (ANA):

 $\begin{array}{rcl} 0.525 \ \text{C}_{2}\text{H}_{3}\text{O}_{2}^{-} + 0.2\text{NH}_{4}^{+} + 0.275\text{H}^{+} & \rightarrow & \text{CH}_{1.8}\text{O}_{0.5}\text{N}_{0.2}^{-} + 0.05\text{HCO}_{3}^{-} + 0.4\text{H}_{2}\text{O}_{1.8}^{-} \\ & \text{biomass} \end{array}$

$$\Delta G_{ANA}^0 = -17.8 \text{ kJ/C-mol biomass}$$
 (at 35°C)
 $v = 0.525 \text{ mol acetate/C-mol biomass}$

Catabolic reaction (CAT):

$$8Fe(OH)_{3} + C_{2}H_{3}O_{2}^{-} + 15H^{+} \rightarrow 8Fe^{2+} + 2HCO_{3}^{-} + 20H_{2}O^{-}$$
$$\Delta G_{CAT}^{0} = -475.9 \text{ kJ/mol acetate} \quad (at 35^{\circ}C)$$

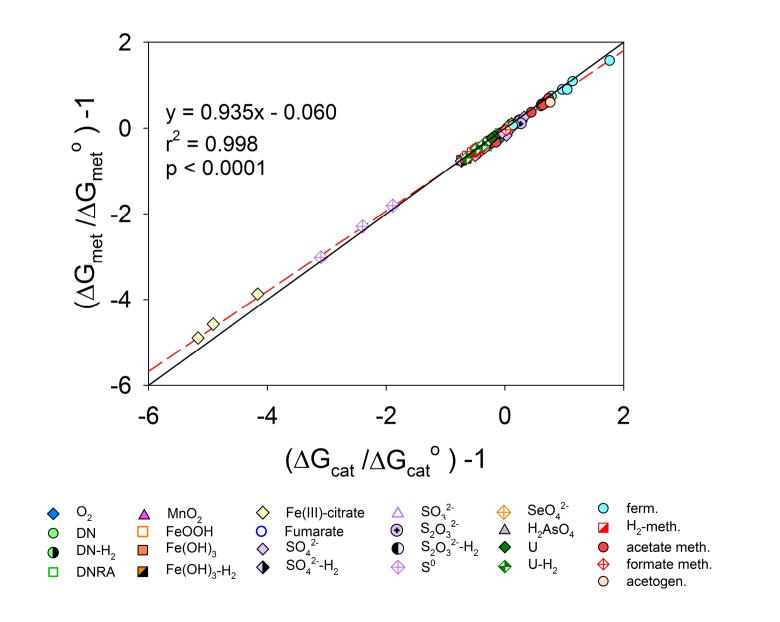
Thermodynamics \rightarrow Growth Yield

$$\lambda_{cat} \left[\text{mol acetate/C-mol biomass} \right]$$
$$Y \left[\text{C-mol biomass/mol acetate} \right]$$

$$\lambda_{\text{cat}} = \frac{1 - Y \cdot v}{Y} \qquad \Delta G_{\text{met}} = \Delta G_{\text{ana}} + \lambda_{\text{cat}} \Delta G_{\text{cat}}$$

$$Y = \frac{\Delta G_{\text{cat}}}{\Delta G_{\text{met}} + \Delta G_{\text{cat}} \cdot \upsilon - \Delta G_{\text{ana}}}$$

Departure from Standard State Conditions



Gibbs Energy Dynamic Yield Method (GEDYM)

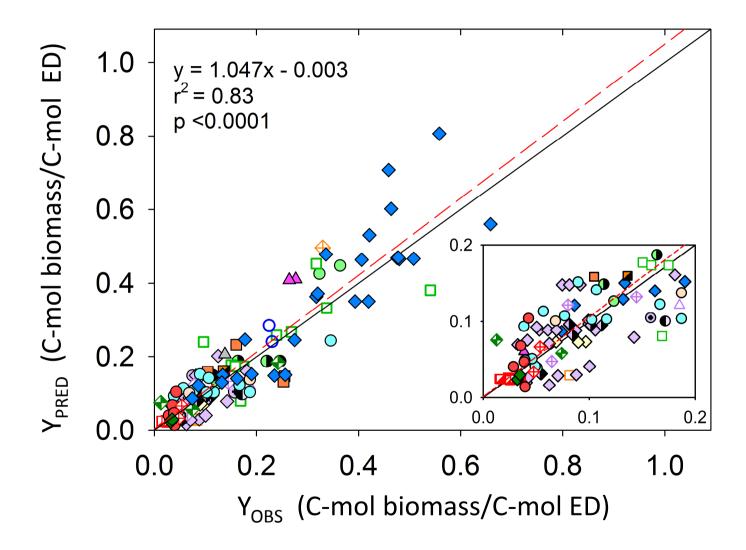
Empirical relationship:

$$\left(\frac{\Delta G_{\text{met}}}{\Delta G_{\text{met}}^{0}} - 1\right) = m \cdot \left(\frac{\Delta G_{\text{cat}}}{\Delta G_{\text{cat}}^{0}} - 1\right) + b$$

Obtain ΔG_{met} and calculate:

$$Y = \frac{\Delta G_{\text{cat}}}{\Delta G_{\text{met}} + \Delta G_{\text{cat}} \cdot \upsilon - \Delta G_{\text{ana}}}$$

Gibbs Energy Dynamic Yield Method (GEDYM)



Experimental Data: Acetate/Fe(OH)₃

Parameters	Units	Value
Physical and C	Chemical:	
Temperature	°C	35
H^{+}	log activity	-7
Acetate	log activity	-1.78
HCO_3^-	log activity	-1.59
Fe^{2+}	log activity	-6.54
Fe(OH) ₃	log activity	1
$\mathrm{NH_4}^+$	log activity	-2.43
Bioenergetic:		
ν	mol ED/C-mol biomass	0.525
$\Delta G_{cat \ 298K}^{\circ}$	kJ/ mol ED	-482.7
$\Delta G_{cat \ 308K}$	kJ/ mol ED	-475.9
$\Delta G_{cat 308K}$	kJ/ mol ED	-173.1
$\Delta G_{an 298K}$	kJ/ C-mol biomass	18.5
$\Delta G_{an 308K}^{"}$	kJ/ C-mol biomass	17.8
$\Delta G_{an 308K}$	kJ/ C-mol biomass	37.0
m		0.9306
b		-0.0690
Predicted Y	C-mol biomass/ C-mol ED	0.105

Experimental conditions: Caccavo et al. (1994) *Geobacter sulfurreducens* sp. nov., a hydrogenand acetate-oxidizing dissimilatory metal-reducing microorganism. *Applied and Environmental Microbiology* **60**, 3752-3759.

Metabolic (Macrochemical) Reaction

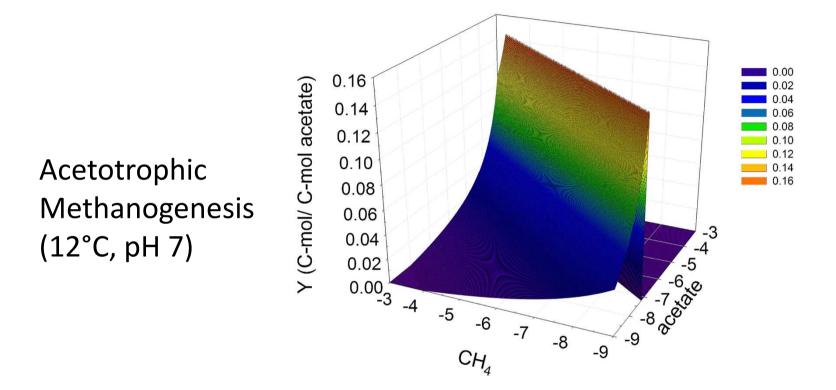
Y = 0.105 C-mol biomass (mol acetate)⁻¹

6.67
$$\operatorname{Fe(OH)}_{_{3}} + \operatorname{C}_{_{2}}\operatorname{H}_{_{3}}\operatorname{O}_{_{2}}^{-} + 0.064 \operatorname{NH}_{_{4}}^{+} + 12.59 \operatorname{H}^{+}$$

 $\rightarrow 0.318 \operatorname{CH}_{_{1.8}}\operatorname{O}_{_{0.5}}\operatorname{N}_{_{0.2}} + 6.67 \operatorname{Fe}^{^{2+}} + 1.68 \operatorname{HCO}_{_{3}}^{-} + 16.79 \operatorname{H}_{_{2}}\operatorname{O}_{_{3}}$

$$\Delta G_{\rm met} = -132.5 \text{ kJ} \text{ (mol acetate)}^{-1}$$

Dynamic Growth Yields



 $C_2H_3O_2^- + H_2O \rightarrow CH_4 + HCO_3^-$

Growth and Maintenance

Pirt Equation:

$$r_{s} = \frac{\mu \cdot X}{Y} + m_{s}$$

where

- r_{s} : substrate utilization rate
- μ : specific growth rate
- X: biomass
- Y : growth yield
- m_s : maintenance requirement (rate)

Bioenergetics and Reactive Transport

- 1. F_T : thermodynamic limitation on catabolic reaction
- 2. λ_{cat} : coupling catabolism and anabolism
- 3. m_e: maintenance requirement

The End



Source: http://www.jantoo.com/cartoon/12265265